

Focus 5: Simple mixtures

TD description of mixtures

Properties of solutions

Phase diagrams of binary systems

Phase diagrams of ternary systems

Thermodynamic activity

Solvent (A) activity

$$(\mu_A = \mu_A^* + RT \ln(p_A/p_A^*))$$

This is the general expression for the chemical potential μ_A of component A in a mixture, where:

- μ_A^* is the chemical potential of pure A (standard state),
- p_A is the partial vapor pressure of A in solution,
- p_A^* is the vapor pressure of pure A,
- R is the gas constant,
- T is temperature.

Solvent (A) activity

$$\mu_A = \mu_A^* + RT \ln x_A$$

Ideal solution

$$(\mu_A = \mu_A^* + RT \ln(p_A/p_A^*))$$


For an ideal solution, the partial pressure of A follows Raoult's Law:

$$p_A = x_A p_A^*$$

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An 'effective' mole fraction that accounts for non-ideal behavior.

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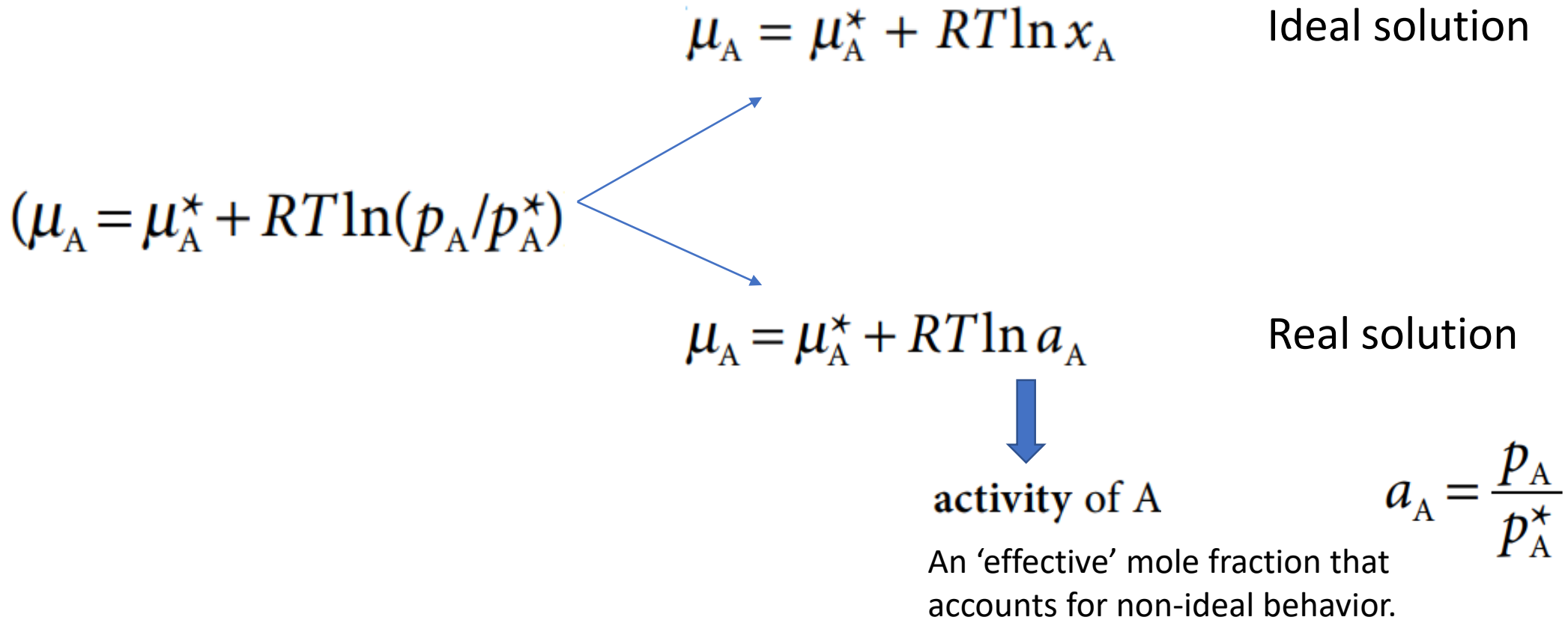
Real solution

activity of A

An 'effective' mole fraction that accounts for non-ideal behavior.

$$a_A = \frac{p_A}{p_A^*}$$

Solvent (A) activity



It adjusts the mole fraction to reflect how the intermolecular environment alters the molecule's escaping tendency!

Solvent activity

The vapour pressure of $0.500 \text{ mol dm}^{-3} \text{ KNO}_3(\text{aq})$ at 100°C is 99.95 kPa , and the vapour pressure of pure water at this temperature is 1.00 atm (101 kPa). It follows that the activity of water in this solution at this temperature is

$$\mu_A = \mu_A^* + RT \ln a_A$$

Real solution



activity of A

An 'effective' mole fraction

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$$a_{\text{A}} = \frac{99.95 \text{ kPa}}{101 \text{ kPa}} = 0.990$$

$$\mu_{\text{A}} = \mu_{\text{A}}^* + RT \ln a_{\text{A}}$$

Real solution



activity of A

An 'effective' mole fraction

$$a_{\text{A}} = \frac{p_{\text{A}}}{p_{\text{A}}^*}$$

Activity Coefficient

$$a_A = \gamma_A x_A$$

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Ideal solution

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Real solution

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Real solution

$$a_A = \gamma_A x_A$$

$$\mu_A = \mu_A^* + RT \ln x_A + RT \ln \gamma_A$$

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Real solution

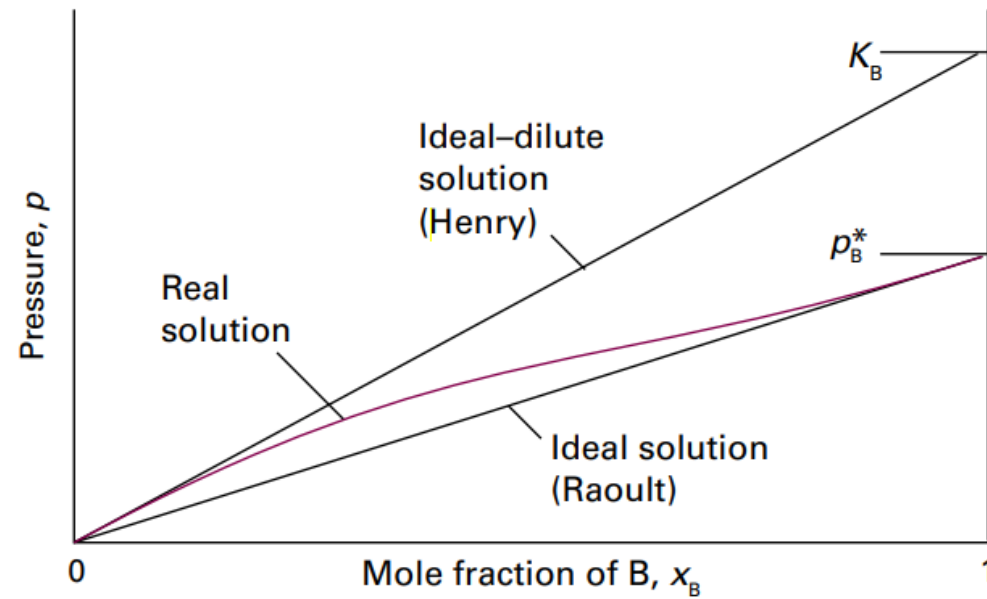
$$a_A = \gamma_A x_A$$

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Ideal solution

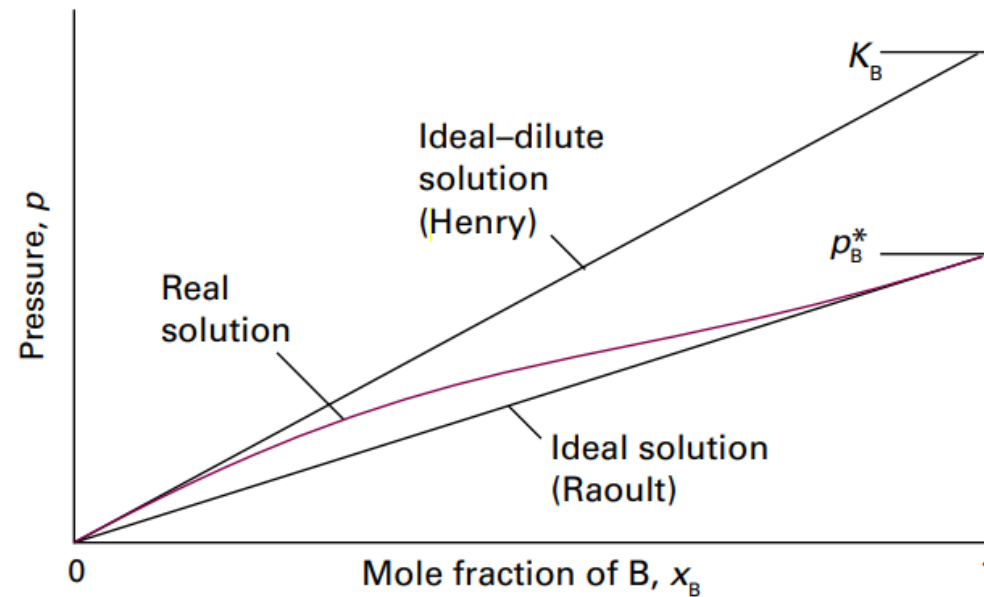
Solute (B) activity

Solute activity in ideal-dilute solutions



Solute activity in ideal-dilute solutions

$$\mu_B = \mu_B^* + RT \ln \frac{p_B}{p_B^*}$$



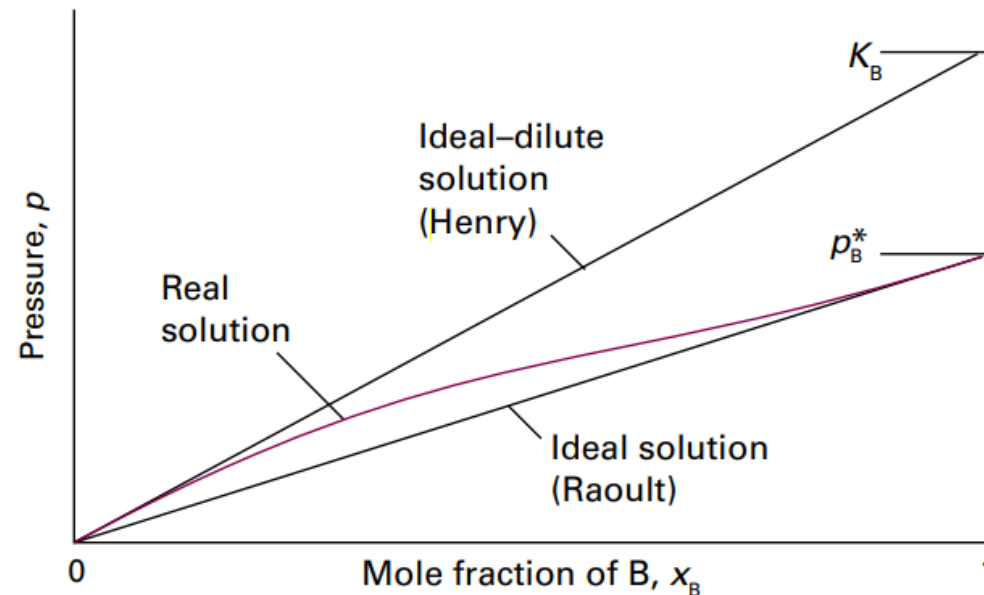
Solute activity in ideal-dilute solutions

$$\mu_B = \mu_B^* + RT \ln \frac{p_B}{p_B^*}$$

Henry's law

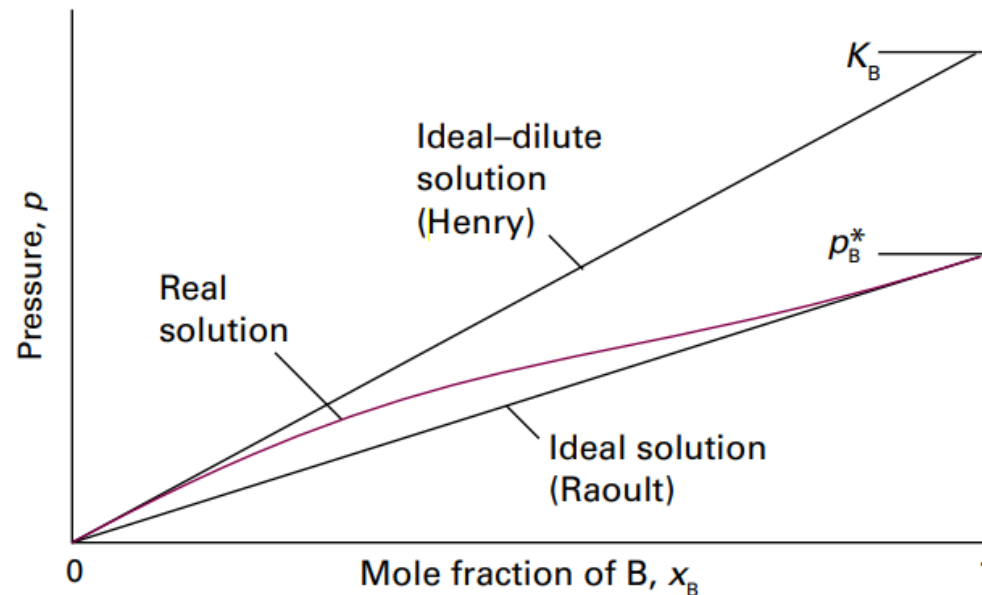
$p_B = K_B x_B$

$$= \mu_B^* + RT \ln \frac{K_B x_B}{p_B^*}$$



Solute activity in ideal-dilute solutions

$$\begin{aligned}\mu_B &= \mu_B^* + RT \ln \frac{p_B}{p_B^*} \\ &\stackrel{\text{Henry's law}}{=} \mu_B^* + RT \ln \frac{K_B x_B}{p_B^*} \\ &= \mu_B^* + RT \ln \frac{K_B}{p_B^*} + RT \ln x_B\end{aligned}$$



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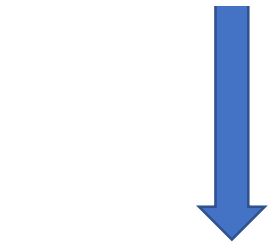
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Where, $\mu_B^\ominus = \mu_B^* + RT \ln \frac{K_B}{p_B^*}$

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Where, $\mu_B^\ominus = \mu_B^* + RT \ln \frac{K_B}{p_B^*}$



If the solution is ideal, $K_B = p_B^*$ (Raoult's law)

$$\mu_B^\ominus = \mu_B^*$$

Solute activity in real solutes

$$\mu_{\text{B}} = \mu_{\text{B}}^{\ominus} + RT \ln x_{\text{B}}$$

In ideal-dilute solutions

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In real solutions



$$a_{\text{B}} = \gamma_{\text{B}} x_{\text{B}}$$

$$a_{\text{B}} = \frac{p_{\text{B}}}{K_{\text{B}}}$$

Example

Use the following information to calculate the activity and activity coefficient of trichloromethane (chloroform, C) in propanone (acetone, A) at 25 °C, treating it first as a solvent and then as a solute.

| | | | | | | |
|------------------|------|------|------|------|------|------|
| x_C | 0 | 0.20 | 0.40 | 0.60 | 0.80 | 1 |
| p_C/kPa | 0 | 4.7 | 11 | 18.9 | 26.7 | 36.4 |
| p_A/kPa | 46.3 | 33.3 | 23.3 | 12.3 | 4.9 | 0 |

$$p_C^* = 36.4 \text{ kPa and } K_C = 23.5 \text{ kPa}$$

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| Case | Standard State | Activity Expression |
|---------|---|---------------------|
| Solvent | Pure liquid ($x \rightarrow 1$) | $a = \frac{p}{p^*}$ |
| Solute | Infinite dilution ($x \rightarrow 0$) | $a = \frac{p}{K}$ |

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From Raoult's law (chloroform regarded as the solvent): (Use Raoult's law as the reference behavior)

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| x_C | 0 | 0.20 | 0.40 | 0.60 | 0.80 | 1 | $a = \frac{p_A}{p_A^*}$ |
| a_C | 0 | 0.13 | 0.30 | 0.52 | 0.73 | 1.00 | |

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| γ_C | | 0.65 | 0.75 | 0.87 | 0.92 | 1.00 | |

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| a_C | 0 | 0.20 | 0.47 | 0.80 | 1.14 | 1.55 | |
| γ_C | | 1.00 | 1.17 | 1.34 | 1.42 | 1.55 | |

Regular solutions

$$H^E \neq 0 \text{ but } S^E = 0.$$

A measure of A-B interactions
compared to A-A and B-B



$$H^E = n\xi RTx_Ax_B$$

$$\xi > 0,$$

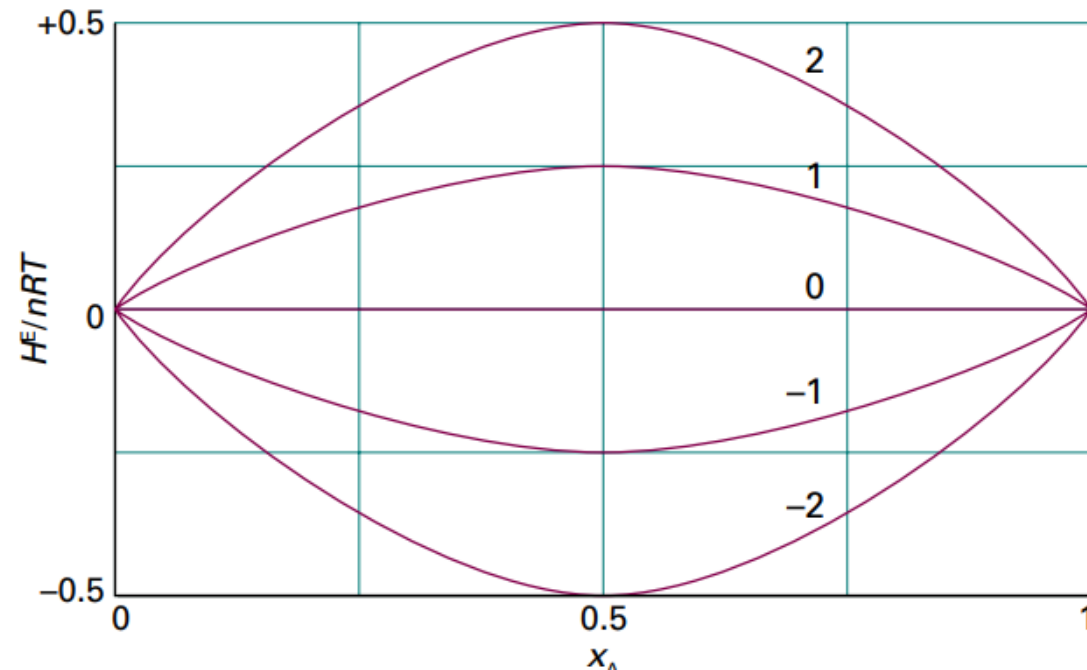
mixing is endothermic.

A-A and B-B interactions are more favorable

$$\xi < 0,$$

mixing is exothermic

A-B interactions are more favorable



Activities of regular solutions

$$\ln \gamma_A = \xi x_B^2$$

- The activity of a component is reduced (or enhanced) depending on how much of the other component is present.

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Similarly, for the other component: $\ln \gamma_B = \xi x_A^2$

Activities of regular solutions

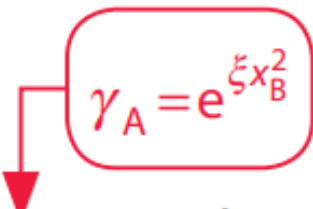
$$\ln \gamma_A = \xi x_B^2 \quad \ln \gamma_B = \xi x_A^2$$

$$\gamma_A \rightarrow 1 \text{ as } x_B \rightarrow 0 \text{ and } \gamma_B \rightarrow 1 \text{ as } x_A \rightarrow 0$$

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$$a_A = \gamma_A x_A = x_A e^{\xi x_B^2}$$

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The diagram illustrates the derivation of the activity a_A for a regular solution. It starts with the equation $a_A = \gamma_A x_A = x_A e^{\xi x_B^2} = x_A e^{\xi (1-x_A)^2}$. A red arrow points from a box containing $\gamma_A = e^{\xi x_B^2}$ to the γ_A term in the equation. Another red arrow points from a box containing $x_B = 1 - x_A$ to the x_B^2 term in the equation.

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The diagram illustrates the derivation of the activity a_A for component A in a regular solution. It starts with the equation $a_A = \gamma_A x_A = x_A e^{\xi x_B^2} = x_A e^{\xi(1-x_A)^2}$. A red arrow points from a box containing $\gamma_A = e^{\xi x_B^2}$ to the γ_A term in the equation. Another red arrow points from a box containing $x_B = 1 - x_A$ to the x_B^2 term in the equation.

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$$p_A = p_A^* x_A e^{\xi(1-x_A)^2}$$

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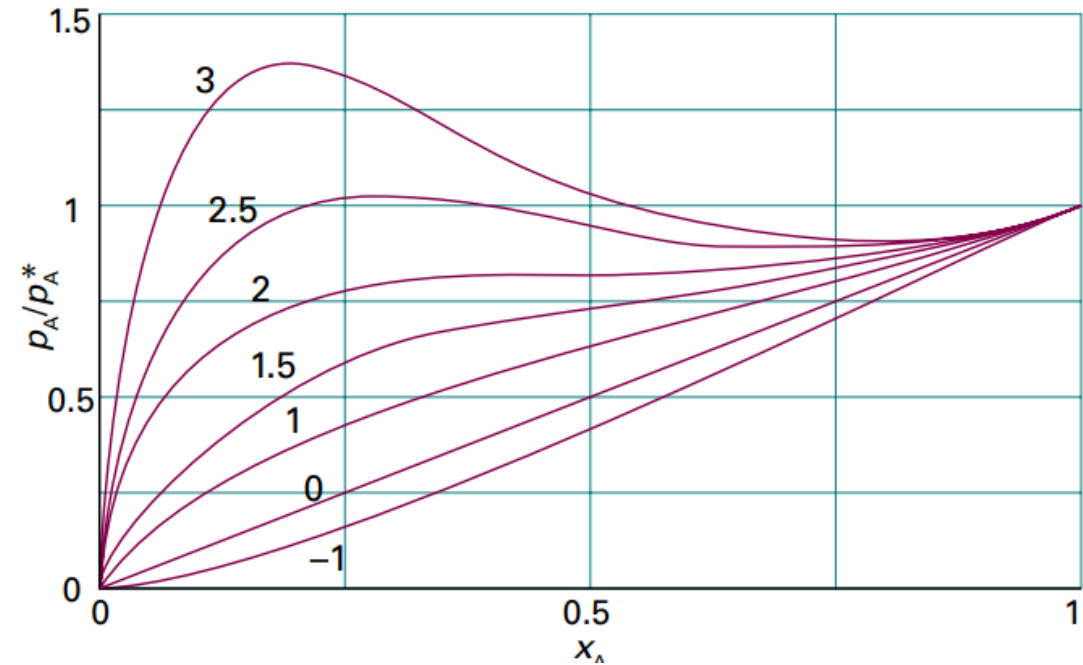
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$\gamma_A = e^{\xi x_B^2}$

$x_B = 1 - x_A$

$$p_A = p_A^* x_A e^{\xi (1-x_A)^2}$$



$$\text{Total vapor pressure} = P_A + P_B$$